

ALFRED BUCHLER AND CARLOS J. HILADO

*Fire Safety Center
University of San Francisco
San Francisco, California 94117*

THE PREDICTION OF TOXIC ATMOSPHERES FROM DECOMPOSING POLYMERS

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ABSTRACT: The generation of carbon monoxide from polymethyl methacrylate and polyethylene, and of hydrogen chloride from polyvinyl chloride, was calculated. Calculations were made for various amounts of polymer evolving gaseous products into a 60 ft³ compartment.

INTRODUCTION

THE PREDICTION OF the amounts of polymeric materials which could be safely exposed to a fire situation in a closed compartment requires a knowledge of the amounts of toxic gases which can be generated from a specific quantity of polymer under particular conditions of exposure. The concentration of toxic gases at any point in time is a function of the quantity of polymer originally present, and of the conditions of temperature and oxygen concentration to which it is exposed.

This paper presents the results of calculations using a computer program to calculate equilibrium compositions of gases from the decomposition of polymethyl methacrylate, polyethylene, and polyvinyl chloride.

COMPUTER PROGRAM

The Aerotherm equilibrium program [1] computes the equilibrium composition and temperature for a chemical system whose initial composition and thermodynamic properties are known. Specifically, the input to the program contains the elemental composition of at most four reactant species (air is counted as a single species) and their enthalpies of formation. The input also contains the elemental composition of all possible product species, gaseous or condensed, their heats of formation and their heat capacities as a function of temperature. The final pressure must also be specified. From these data, the program calculates the equilibrium composition and temperature of the system, the temperature corresponding to the adiabatic flame temperature in the case of a combustion reaction.

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POLYMETHYL METHACRYLATE

Our model assumes that polymethyl methacrylate (PMMA) is first pyrolyzed to give the gaseous monomer [2]. The latter then reacts with varying amounts of oxygen in air to give the equilibrium combustion products (Table 1). The pyrolysis kinetics provide the rate-determining step, the rate constant being taken from Madorsky [2]. The carbon monoxide concentrations produced in a 60 ft³ closed compartment by the pyrolysis and burning of 10, 20, and 50 g quantities of PMMA are shown in Tables 2 to 4 and in Figures 1 to 3.

The individual figures correspond to PMMA combustion in air with oxygen/PMMA monomer mole ratios of 2:1, 5:1, and 6:1. In each case, curves of CO concentration as a function of time are given for PMMA pyrolysis temperatures ranging from 340 to 400°C. Higher pyrolysis temperatures generally increase the rate of production of CO, with the 60°C temperature interval corresponding to a 50-fold rate increase for the case of a 2:1 mole ratio of oxygen to PMMA monomer. The latter case produces the most toxic effects in terms of CO generation. For 10 g PMMA, the maximum concentration possible is close to 6,000 ppm; this concentration is almost reached in 2 min with a pyrolysis temperature of 400°C (Figure 1). For the same 2:1 ratio, the pyrolysis and combustion of 50 g PMMA at a pyrolysis temperature of 340°C produces nearly 9,000 ppm CO, the lower temperature being more than compensated for by the larger amount of PMMA and the longer time.

Less CO is produced at the higher oxygen/PMMA ratios (Figures 2 and 3). The maximum concentration possible for 10 g PMMA is about 2,200 ppm CO for a ratio of 5:1, and 700 ppm for a ratio of 6:1. With the 5:1 ratio, the CO concentration

Table 1. Combustion of Polymethyl Methacrylate (PMMA) in Air.

Moles oxygen/mole PMMA monomer	2	5	6
Equilibrium composition (mole fractions)			
carbon monoxide (CO)	0.273	0.060	0.016
carbon dioxide (CO ₂)	0.030	0.119	0.140
water (H ₂ O)	0.030	0.130	0.121
hydrogen (H ₂)	0.212	0.012	0.003
oxygen (O ₂)	0.000	0.000	0.007
nitrogen (N ₂)	0.455	0.675	0.705
hydroxyl (OH)	0.000	0.001	0.003
nitric oxide (NO)	0.000	0.000	0.003
Moles CO/mole PMMA monomer	4.5	1.7	0.5
Temperature, °K.	1181	2235	2278

Table 2. Generation of Carbon Monoxide from Polymethyl Methacrylate Oxygen/
PMMA Monomer Ratio 2:1 — Compartment Volume 60 ft³

Temperature °C.	Time min	CO Concentration, ppm		
		10 g PMMA	20 g PMMA	50 g PMMA
340	1	403	803	2,015
	2	784	1,568	3,920
	5	1,770	3,540	8,850
	10	3,012	6,024	15,060
	20	4,497	8,994	22,485
	50	5,768	11,536	28,840
350	1	772	1,544	3,860
	2	1,426	2,852	7,130
	5	2,982	5,964	14,910
	10	4,466	8,932	22,330
	20	5,578	11,156	27,890
	50	5,934	11,868	29,670
360	1	1,428	2,816	7,040
	2	2,477	4,954	12,385
	5	4,402	8,804	22,010
	10	5,542	11,084	27,710
	20	5,910	11,820	29,550
	50	5,940	11,880	29,700
370	1	2,376	4,752	11,880
	2	3,802	7,604	19,010
	5	5,477	10,954	27,385
	10	5,904	11,808	29,520
	20	5,940	11,880	29,700
380	1	3,641	7,282	18,205
	2	5,049	10,098	25,245
	5	5,887	11,774	29,435
	10	5,940	11,880	29,700
390	1	4,889	9,778	24,445
	2	5,756	11,512	28,780
	5	5,940	11,880	29,700
400	1	5,673	11,346	28,365
	2	5,928	11,856	29,640
	5	5,940	11,880	29,700
maximum		5,940	11,880	29,700

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*Table 3. Generation of Carbon Monoxide from Polymethyl Methacrylate Oxygen/
PMMA Monomer Ratio 5:1 - Compartment Volume 60 ft³*

Temperature °C.	Time min	CO Concentration, ppm		
		10 g PMMA	20 g PMMA	50 g PMMA
340	1	152	304	760
	2	296	592	1,480
	5	668	1,336	3,340
	10	1,136	2,272	5,680
	20	1,696	3,392	8,480
	50	2,175	4,350	10,875
350	1	291	582	1,455
	2	547	1,094	2,735
	5	1,125	2,250	5,625
	10	1,685	3,370	8,425
	20	2,104	4,208	10,522
	50	2,238	4,476	11,190
360	1	531	1,062	2,655
	2	934	1,868	4,670
	5	1,660	3,320	8,300
	10	2,090	4,180	10,450
	20	2,229	4,458	11,145
	50	2,240	4,480	11,200
370	1	896	1,792	4,480
	2	1,434	2,868	7,170
	5	2,066	4,132	10,330
	10	2,227	4,454	11,135
	20	2,240	4,480	11,200
380	1	1,373	2,746	6,865
	2	1,904	3,808	9,520
	5	2,220	4,440	11,100
	10	2,240	4,480	11,200
390	1	1,844	3,688	9,220
	2	2,171	4,342	10,855
	5	2,240	4,480	11,200
400	1	2,139	4,278	10,695
	2	2,236	4,472	11,180
	5	2,240	4,480	11,200
maximum		2,240	4,480	11,200

Table 4. Generation of Carbon Monoxide from Polymethyl Methacrylate Oxygen/
PMMA Monomer Ratio 6:1 — Compartment Volume 60 ft³

Temperature °C.	Time min	CO Concentration, ppm		
		10 g PMMA	20 g PMMA	50 g PMMA
340	1	46	92	230
	2	89	178	445
	5	200	400	1,000
	10	341	682	1,705
	20	509	1,018	2,545
	50	653	1,306	3,265
350	1	87	174	435
	2	161	322	805
	5	338	676	1,690
	10	506	1,012	2,530
	20	632	1,264	3,160
	50	672	1,344	3,360
360	1	159	318	795
	2	286	562	1,425
	5	499	998	2,495
	10	628	1,256	3,140
	20	669	1,338	3,345
	50	673	1,346	3,365
370	1	269	538	1,345
	2	431	862	2,155
	5	620	1,240	3,100
	10	669	1,338	3,345
	20	673	1,346	3,365
380	1	412	824	2,060
	2	572	1,144	2,860
	5	667	1,334	3,335
	10	673	1,346	3,365
390	1	554	1,108	2,770
	2	652	1,304	3,260
	5	673	1,346	3,365
400	1	643	1,286	3,215
	2	671	1,342	3,355
	5	673	1,346	3,365
maximum		673	1,346	3,365

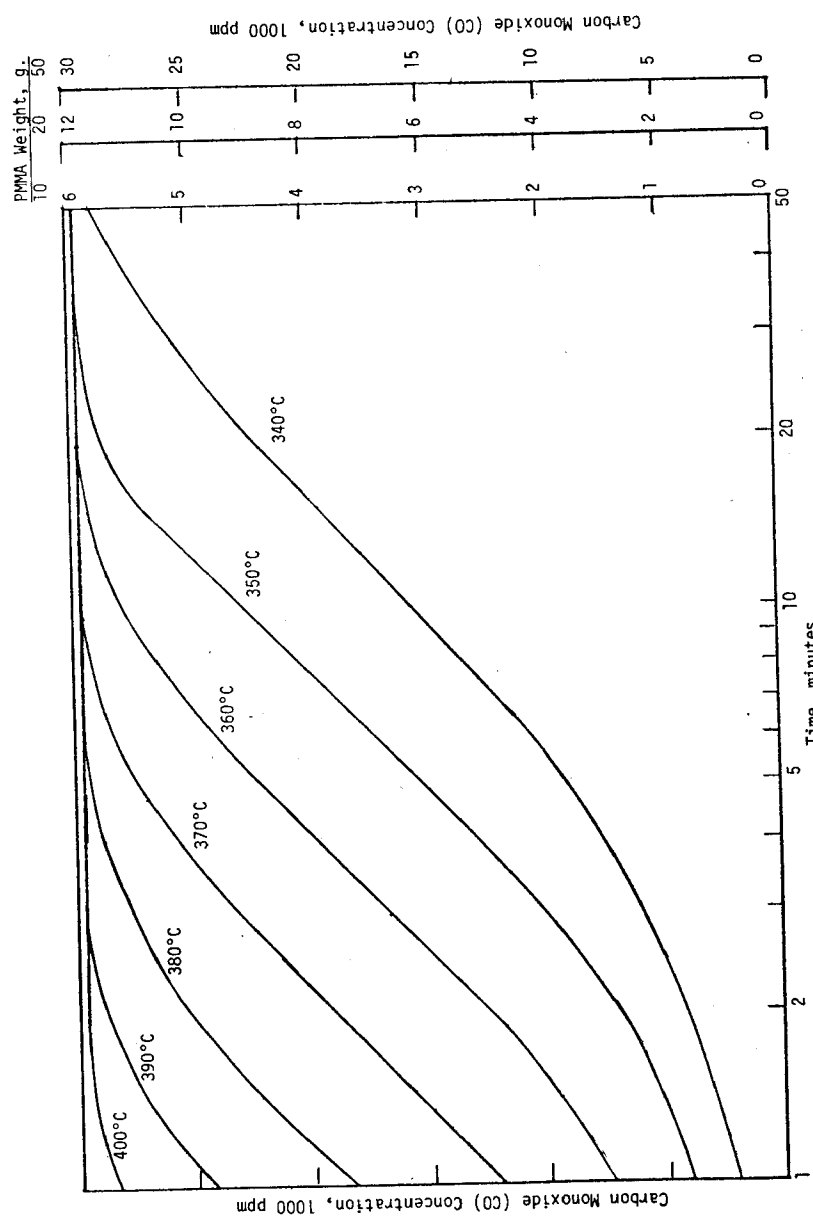


Figure 1. Generation of Carbon Monoxide from Polymethyl Methacrylate (2:1 O₂/PMMA).

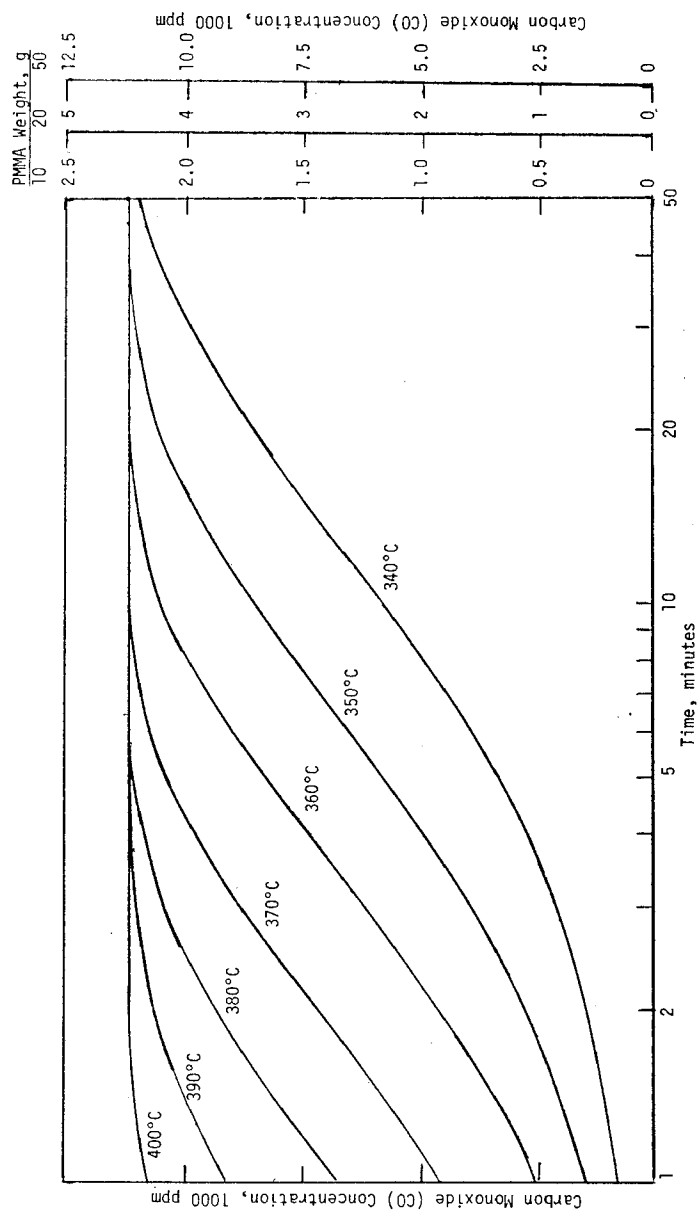


Figure 2. Generation of Carbon Monoxide from Polymethyl Methacrylate (5:1 O₂/PMMA).

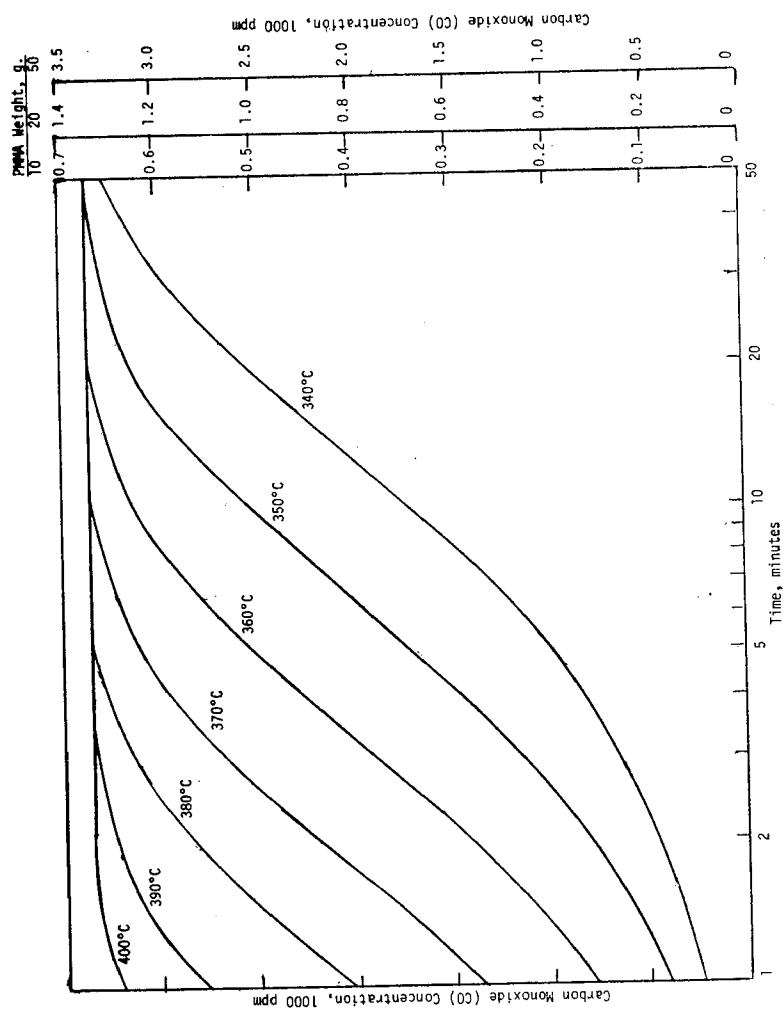


Figure 3. Generation of Carbon Monoxide from Polymethyl Methacrylate (6:1 O₂/PMMA).

reaches 3,000 ppm only with a 50 g quantity of PMMA. With increasing availability of oxygen the toxic threat decreases, but the temperature and hence the thermal threat increase.

POLYETHYLENE

In the case of polyethylene, the situation is more complicated, at 600°C, there are four major volatile decomposition products, with 60 per cent of the volatile material being monomeric ethylene [3]. At lower temperatures there is a wide range of products with very little or no ethylene [2]. Nevertheless, we have carried out calculations for a model in which ethylene is the only decomposition product at all temperatures. The main effect of this assumption is to make the calculated equilibrium temperatures somewhat too high. The calculated equilibrium compositions (Table 5) will still reflect correctly the trend produced by the varying carbon/oxygen ratio. The rate constant for the pyrolysis of linear polyethylene was taken from the work of Wall [4].

The carbon monoxide concentrations produced in a 60 ft³ closed compartment by the pyrolysis and burning of 10, 20, and 50 g quantities of polyethylene are shown in Tables 6 and 7 and in Figures 4 and 5.

The individual figures correspond to oxygen/polyethylene monomer ratios of 1:1 and 3:1. The temperatures are higher than in the case of PMMA, ranging from 470 to 530°C. Carbon monoxide concentrations are given as a function of time for polymer weights of 10, 20 and 50 g. The maximum CO concentrations in a 60 ft³

Table 5. Combustion of Polyethylene (PE) in Air.

Moles oxygen/mole PE monomer	1	3
Equilibrium composition (mole fractions)		
carbon monoxide (CO)	0.257	0.020
carbon dioxide (CO ₂)	0.000	0.109
water (H ₂ O)	0.000	0.122
hydrogen (H ₂)	0.257	0.004
oxygen (O ₂)	0.000	0.009
nitrogen (N ₂)	0.485	0.726
hydroxyl (OH)	0.000	0.004
nitric oxide (NO)	0.000	0.005
Moles CO/mole PE monomer	2.0	0.3
Temperature, °K.	1420	2370

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Table 6. Generation of Carbon Monoxide from Polyethylene Oxygen/PE Monomer Ratio 1:1 — Compartment Volume 60 ft³.

Temperature °C.	Time min	CO Concentration, ppm		
		10 g PE	20 g PE	50 g PE
470	1	498	996	2,490
	2	969	1,938	4,845
	5	2,239	4,478	11,195
	10	3,951	7,902	19,755
	20	6,236	12,472	31,180
	50	8,785	17,570	43,925
480	1	931	1,862	4,655
	2	1,759	3,518	8,795
	5	3,809	7,618	19,045
	10	6,076	12,152	30,380
	20	8,230	16,460	41,150
	50	9,350	18,700	46,750
490	1	1,655	3,310	8,275
	2	3,019	6,038	15,095
	5	5,841	11,682	29,205
	10	8,051	16,102	40,255
	20	9,208	18,416	46,040
	50	9,406	18,812	47,030
500	1	2,822	5,644	14,110
	2	4,797	9,594	23,985
	5	7,826	15,652	39,130
	10	9,142	18,284	45,710
	20	9,397	18,794	46,985
	50	9,406	18,812	47,030
510	1	4,487	8,974	22,435
	2	6,829	13,658	34,145
	5	9,039	18,078	45,195
	10	9,387	18,774	46,935
	20	9,406	18,812	47,030
520	1	6,434	12,868	32,170
	2	8,465	16,930	42,325
	5	9,378	18,756	46,890
	10	9,406	18,812	47,030
530	1	8,174	16,348	40,870
	2	9,246	18,492	46,230
	5	9,406	18,812	47,030
maximum		9,406	18,812	47,030

Table 7. Generation of Carbon Monoxide from Polyethylene Oxygen/PE Monomer Ratio 3:1 — Compartment Volume 60 ft³.

Temperature °C.	Time min	CO Concentration, ppm		
		10 g PE	20 g PE	50 g PE
470	1	75	150	375
	2	146	292	730
	5	336	672	1,680
	10	593	1,186	2,965
	20	936	1,872	4,680
	50	1,318	2,636	6,590
480	1	140	280	700
	2	264	528	1,320
	5	572	1,144	2,860
	10	912	1,824	4,560
	20	1,235	2,470	6,175
	50	1,403	2,806	7,015
490	1	249	498	1,245
	2	453	906	2,265
	5	876	1,752	4,380
	10	1,208	2,416	6,040
	20	1,382	2,764	6,910
	50	1,411	2,822	7,055
500	1	424	848	2,120
	2	720	1,440	3,600
	5	1,174	2,348	5,870
	10	1,372	2,744	6,860
	20	1,410	2,820	7,050
	50	1,411	2,822	7,055
510	1	673	1,346	3,365
	2	1,025	2,050	5,125
	5	1,356	2,712	6,780
	10	1,408	2,816	7,040
	20	1,411	2,822	7,055
520	1	965	1,930	4,825
	2	1,270	2,540	6,350
	5	1,407	2,814	7,035
	10	1,411	2,822	7,055
530	1	1,226	2,452	6,130
	2	1,387	2,774	6,935
	5	1,411	2,822	7,055
maximum		1,411	2,822	7,055

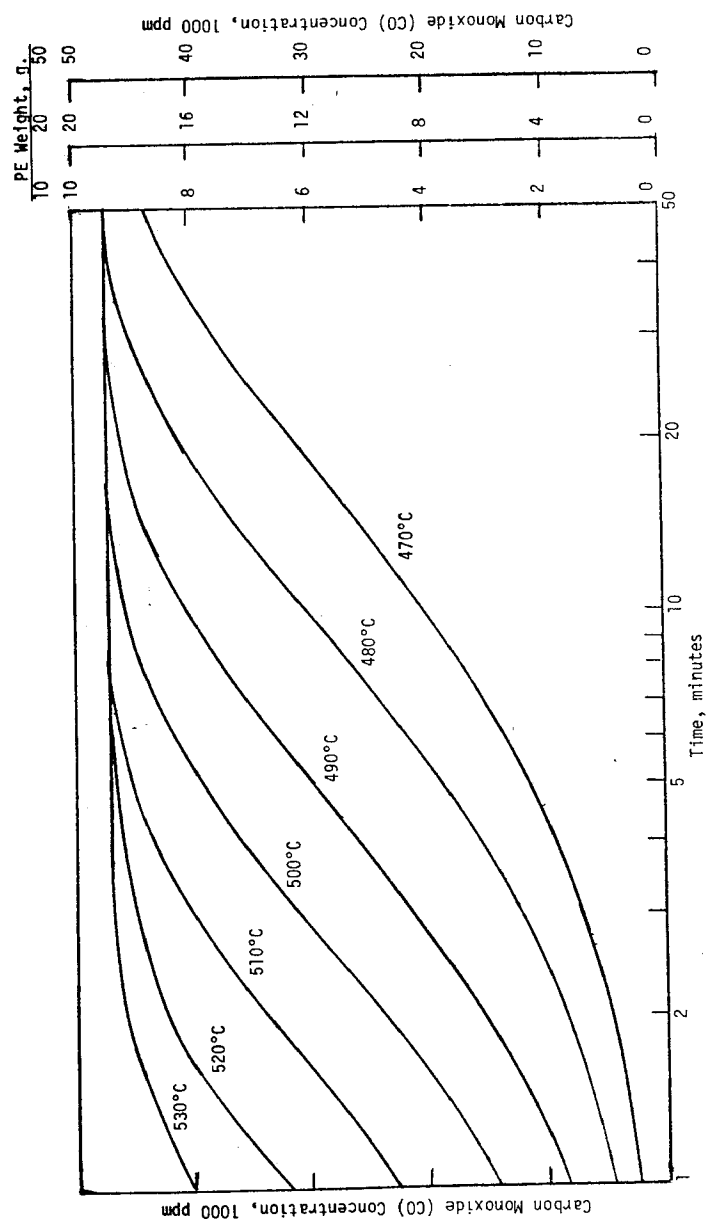


Figure 4. Generation of Carbon Monoxide from Polyethylene (1:1 O₂/PE).

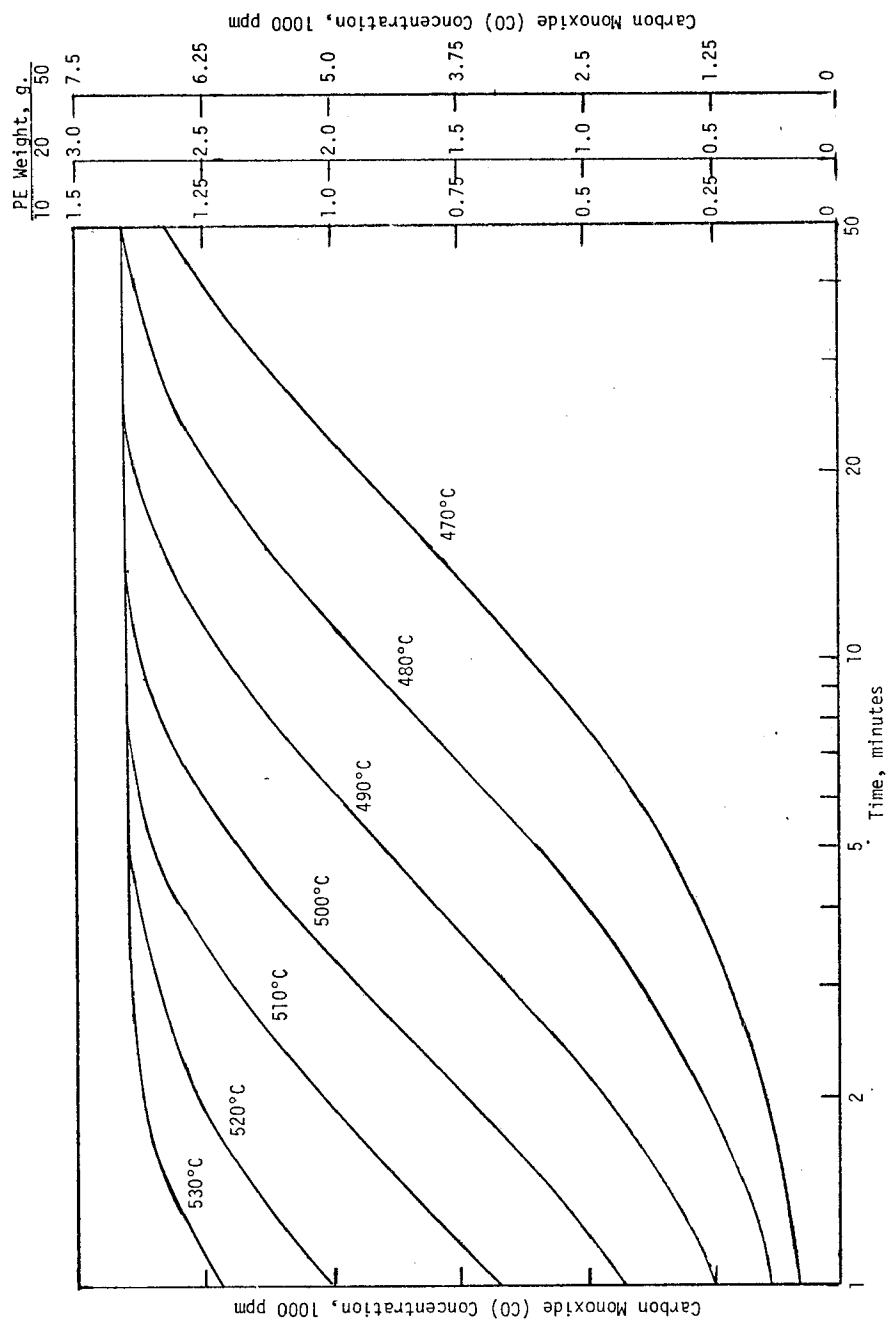


Figure 5. Generation of Carbon Monoxide from Polyethylene (2:1 O₂/PE).

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Table 8. Generation of Hydrogen Chloride from Polyvinyl Chloride: Compartment Volume 60 ft³.

Temperature °C.	Time min	HCl Concentration, ppm		
		10 g PVC	20 g PVC	50 g PVC
240	1	16.5	33	82.5
	2	33	66	165
	5	82.5	165	413
	10	165	330	825
	20	339.5	679	1,698
	50	1,382	2,764	6,910
250	1	30.2	60.5	151
	2	60.5	121	303
	5	151.5	303	758
	10	306	612	1,530
	20	751	1,502	3,755
	50	2,006	4,013	10,033
260	1	55	110	275
	2	110	220	550
	5	275	550	1,375
	10	588	1,177	2,943
	20	1,502	3,005	7,513
	50	2,108	4,216	10,540
270	1	96	192	480
	2	192	384	960
	5	481	962	2,405
	10	1,086	2,173	5,433
	20	2,004	4,009	10,023
	50	2,110	4,220	10,550
280	1	166.5	333	833
	2	333.5	667	1,668
	5	880	1,760	4,400
	10	1,794	3,587	8,968
	20	2,089	4,178	10,445
	50	2,110	4,220	10,550
290	1	280.5	561	1,403
	2	561	1,122	2,805
	5	1,473	2,946	7,365
	10	2,065	4,130	10,325
	20	2,110	4,220	10,550
300	1	470	939	2,348
	2	939	1,878	4,695
	5	1,938	3,877	9,692
	10	2,108	4,216	10,540
	20	2,110	4,220	10,550
maximum		2,110	4,220	10,550

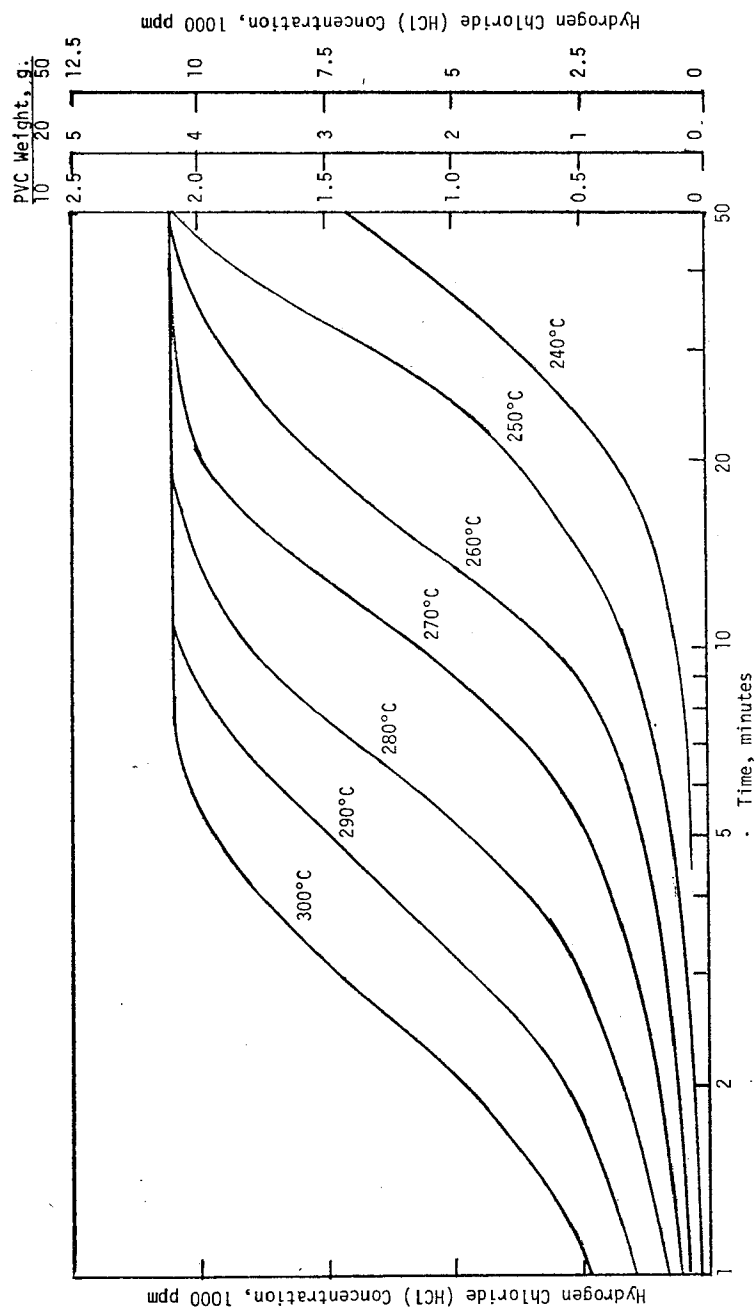


Figure 6. Generation of Hydrogen Chloride from Polyvinyl Chloride.

chamber produced by a 10 g quantity of polyethylene are about 9,400 ppm for the 1:1 ratio, and 1,400 ppm for the 3:1 ratio. In many respects, the behavior of polyethylene is analogous to that of PMMA. A similar pattern may be expected for any polymer which pyrolyzes to give volatile hydrocarbon products.

POLYVINYL CHLORIDE

The behavior of polyvinyl chloride (PVC) differs from that of polymethyl methacrylate and polyethylene in that the toxic gas produced is hydrogen chloride instead of carbon monoxide, and pyrolysis alone is sufficient to produce the toxic gas without the necessity for combustion.

The hydrogen chloride (HCl) concentrations in a 60 ft³ closed compartment produced by pyrolysis of PVC at temperatures ranging from 240 to 300°C are shown in Table 8 and in Figure 6. HCl concentrations are shown as a function of time for 10, 20, and 50 g quantities of PVC. The maximum possible HCl concentration produced by 10 g PVC is about 2,100 ppm.

The rate equations for the dehydrochlorination of PVC were taken from the work of Taliadini and Pezzin [5].

CONCLUSIONS

Small differences in pyrolysis temperature in a temperature region that is critical for a particular polymer can result in substantial changes in toxic gas generation. This critical temperature is approximately 360°C for polymethyl methacrylate, 500°C for polyethylene, and 270°C for polyvinyl chloride.

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