

# *Thermochemical Flammability Model for Thin Materials*

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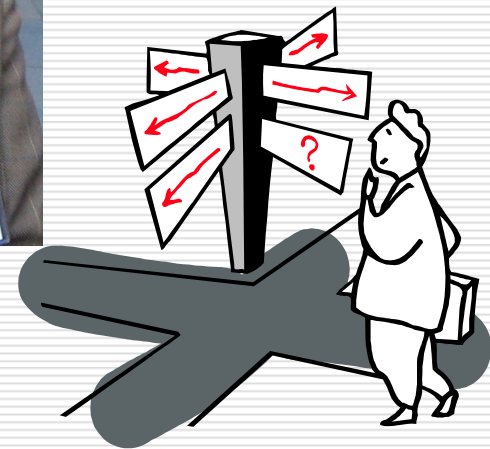
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# Outline

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- ❑ Objective
- ❑ Background
- ❑ TGA Analysis
- ❑ DSC Analysis
- ❑ Modeling
- ❑ Results of Modeling
- ❑ Conclusions



# Objective

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- The goal of this research is to predict the burning of thermally thin materials by modeling.
  - To provide the needed data for the model, TGA and DSC analysis have been performed
  - The materials and the data of Liu with pure nylon and nylon with 5% clay additive, conducted in the Cone Calorimeter will be used for comparison
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# Background-1

- Burning behavior differs according to thickness & heat flux.
  - ✓ Thermally thick burning
  - ✓ Thermally thin burning
  
- Material flammability of nano-clay loading
  - ✓ Ignition time increased
  - ✓ The burning rate greatly reduced

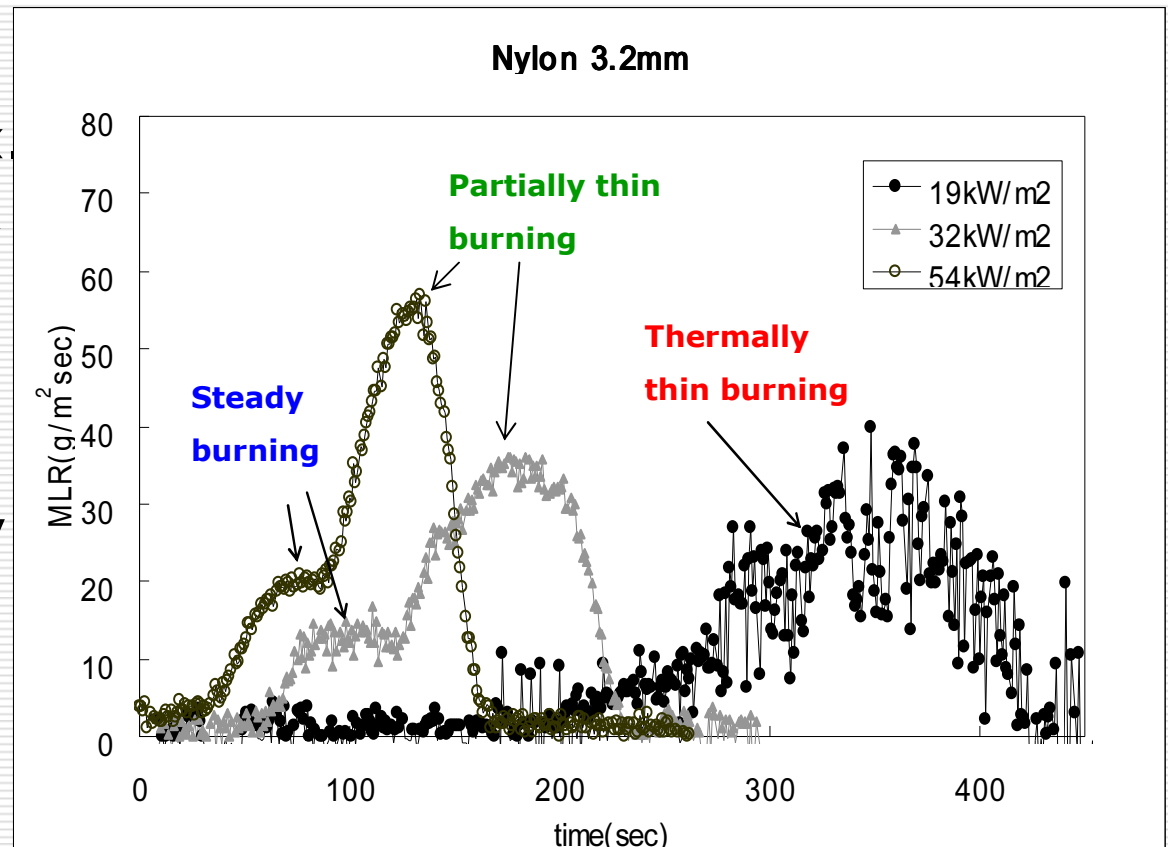


Fig.1 Thermally thick & thin burning

## Background-2

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- For modeling
    - It's very important to understand **the decomposition effects** in the burning of thermally thin material
  
  - Is it **possible to use TGA/DSC for predicting** the burning behavior?
    - The heating rate( $\beta$ ) of TGA & DSC : 0.1~30 K/min  
The heating rate of fires :100 K/min or greater
  
    - $E_a$  &  $a_p$  derived from TGA change with heating rate.  
TGA's relevance to fires has been questioned. Hence, this study will attempt to examine the use of TGA and DSC data in the thermally thin model for fire application
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## Definition and TGA data

- A technique in which the mass of a substance is measured as a function of temperature while the substance is subjected to a controlled temperature program

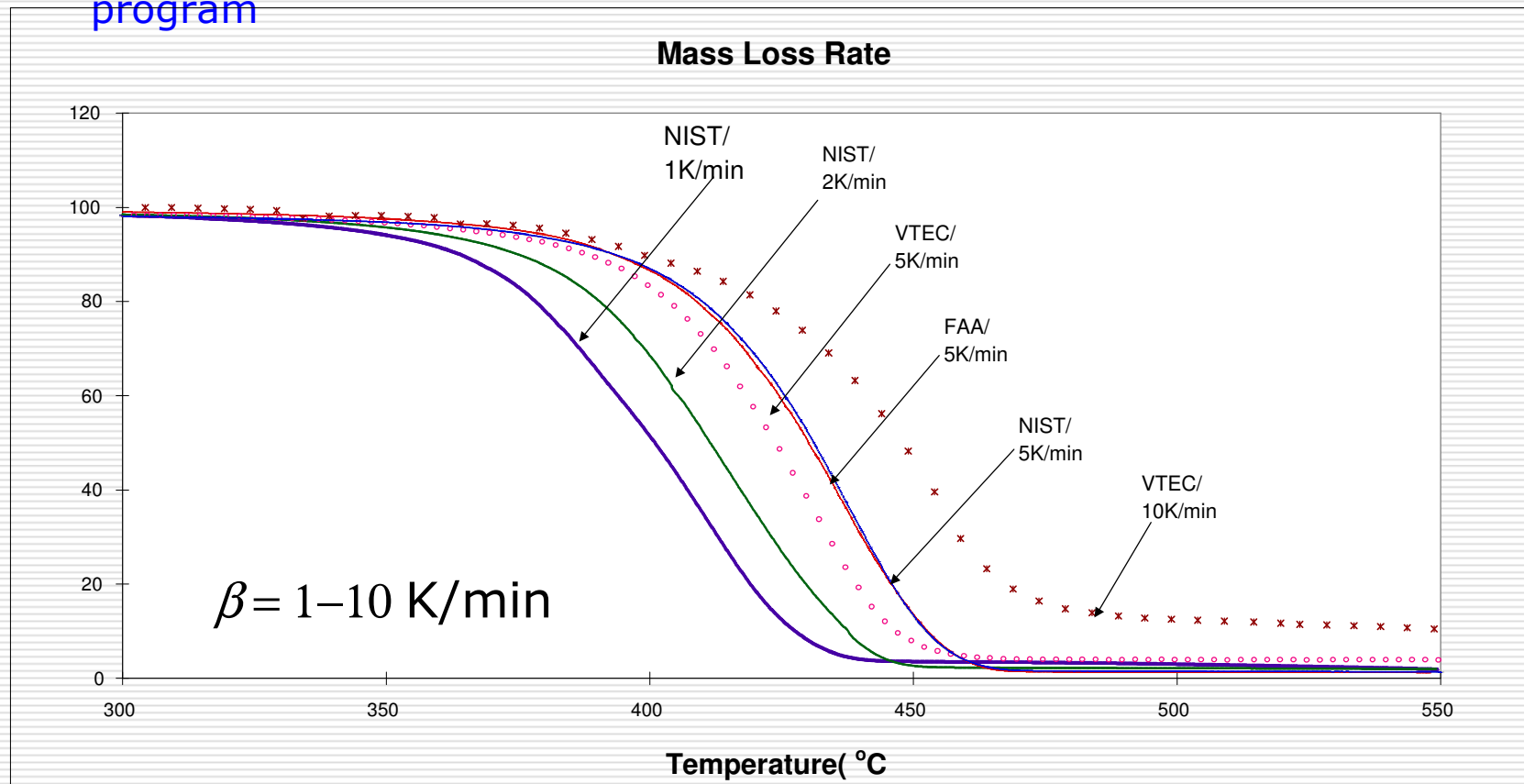


Figure 2. TGA curves of Nylon obtained from experiment

# The Kinetics

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- The thermal decomposition of the solid is assumed to follow **first-order Arrhenius reaction**

$$\frac{d\alpha}{dt} = \frac{(1-\alpha)}{(1-X_c)} a_p e^{-E_a/RT}$$

This is the basic equation needed in our TGA analysis **to determine the kinetic parameters,**

**$E_a$  and  $a_p$**

- ✓ Conversion factor,  $\alpha = \frac{m - m_i}{m_f - m_i} = \frac{m/m_i - 1}{X_c - 1}$

- ✓ Char fraction,  $X_c = \frac{m_f}{m_i}$

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# TGA analysis method

□ Eqn (2.19)

$$\ln\left(\frac{d\alpha}{dt}\right) = \ln\left\{\frac{(1-\alpha)}{(1-X_c)} \times a_p\right\} - \frac{E_a}{R} \left(\frac{1}{T}\right)$$

✓  $E_a$  changes with heating rate and  $\alpha$

The trend: as  $\alpha \uparrow$ ,  $E_a \uparrow$

✓ Slope =  $-E_a/R$ ,

✓ Intercept =  $\ln\left[\frac{(1-\alpha)}{(1-X_c)} a_p\right]$

✓ Kinetic parameter determined

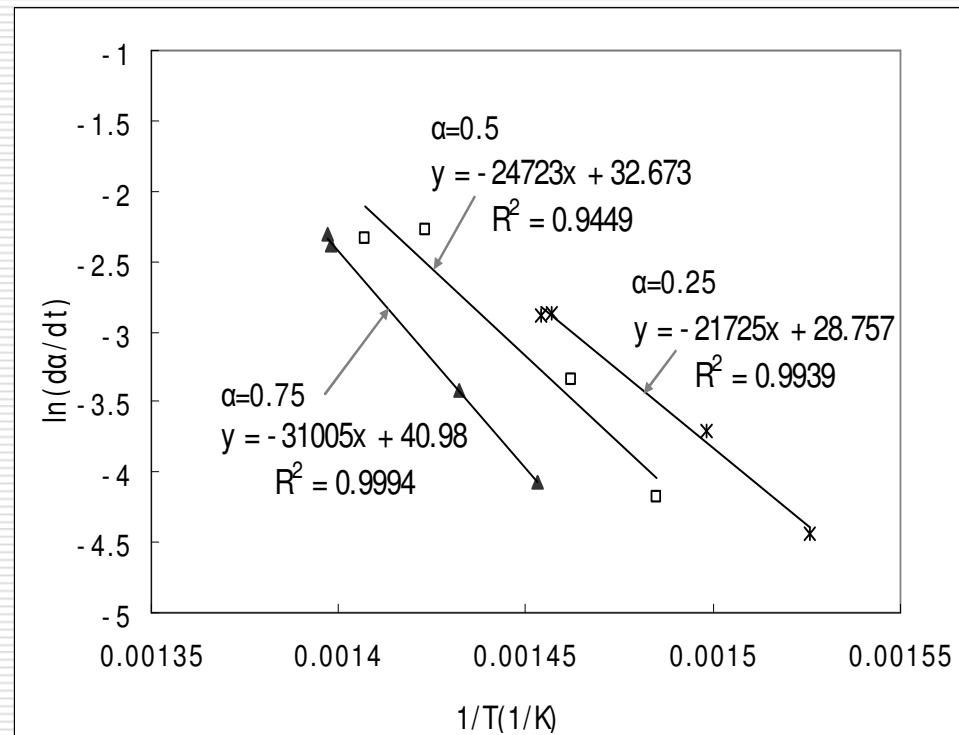


Figure 3. Determining  $E_a$  and  $a_p$  of Nylon



# Results of TGA modeling

Table 2-4. Kinetic parameters

Material	Activation energy ( $E_a$ )	Pre-Exponential factor ( $a_p$ )
Nylon	223 kJ/mol	$1.5 \times 10^{14} \text{ s}^{-1}$
Nylon+5%	223 kJ/mol	$2.1 \times 10^{14} \text{ s}^{-1}$

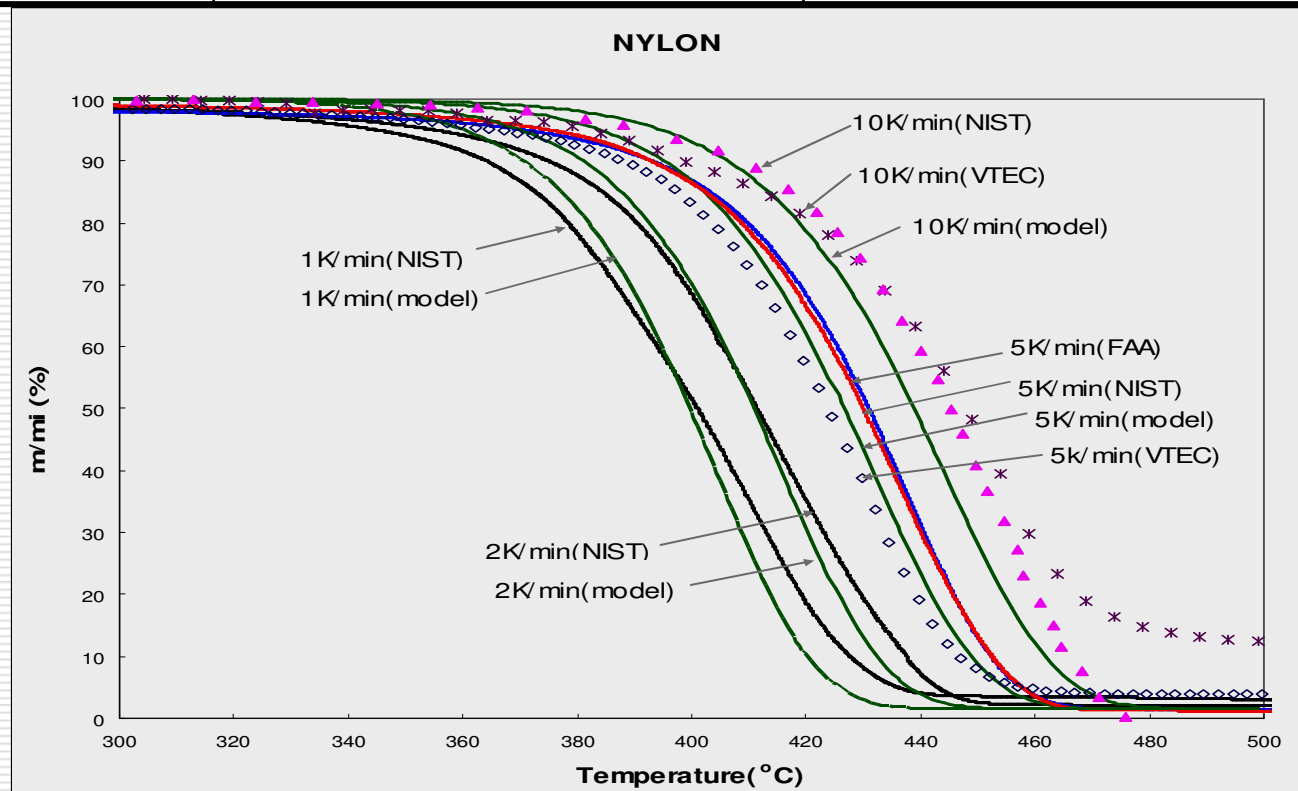


Figure 4. Comparing the model to the experiment

# Definition and use of DSC

- ❑ DSC measures the difference in energy inputs into substance and reference material as a function of temperature while these are subjected to a controlled temperature program
- ✓ The difference of power supplies between two cups shows that  $C_p$ ,  $Q_m$  and  $Q_p$
- ✓ The interpretation ultimately relies on a careful procedure involving the establishment of a “baseline” signal for no sample,
- ✓ and a special procedure to evaluate the heat loss between the heater-cup system and flowing gas
- ✓ Big help from FAA

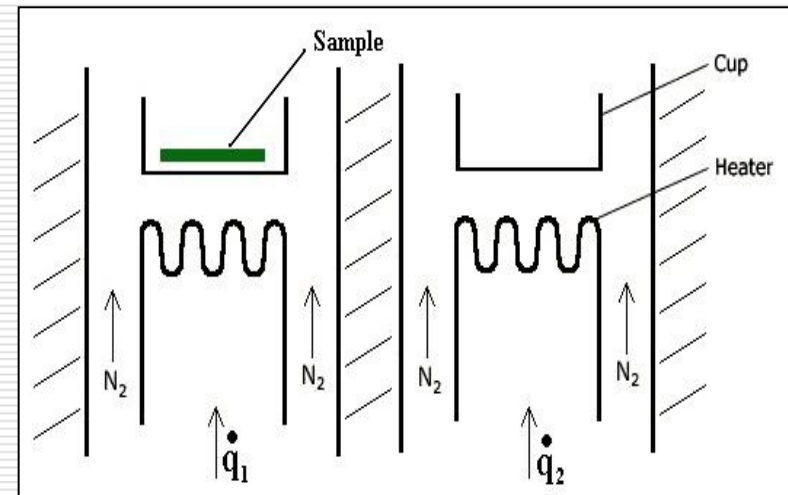


Figure5. Schematic of heat transfer in DSC

# DSC data

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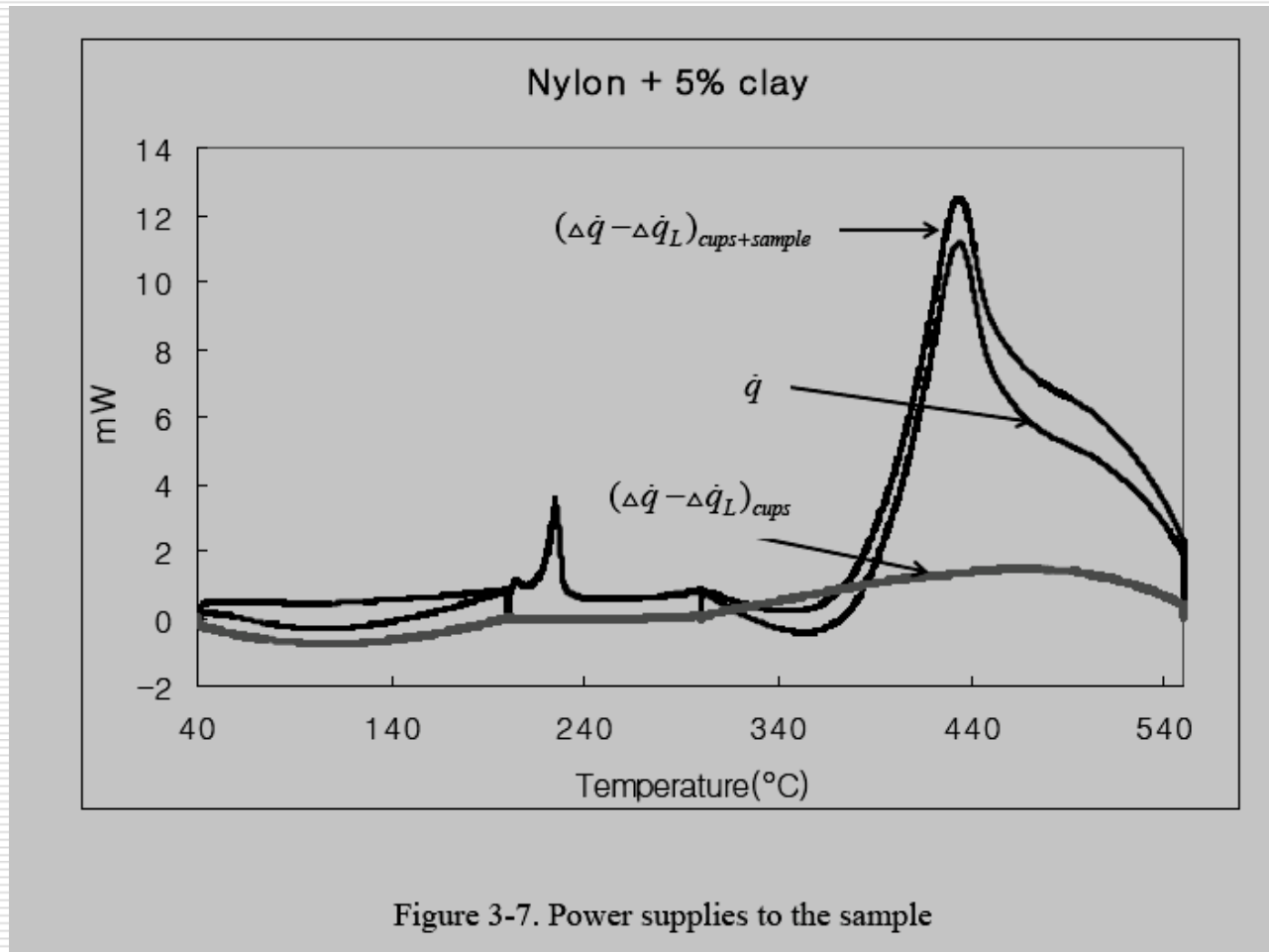


Figure 6. Power supplies to the sample

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# Results of DSC analysis-1

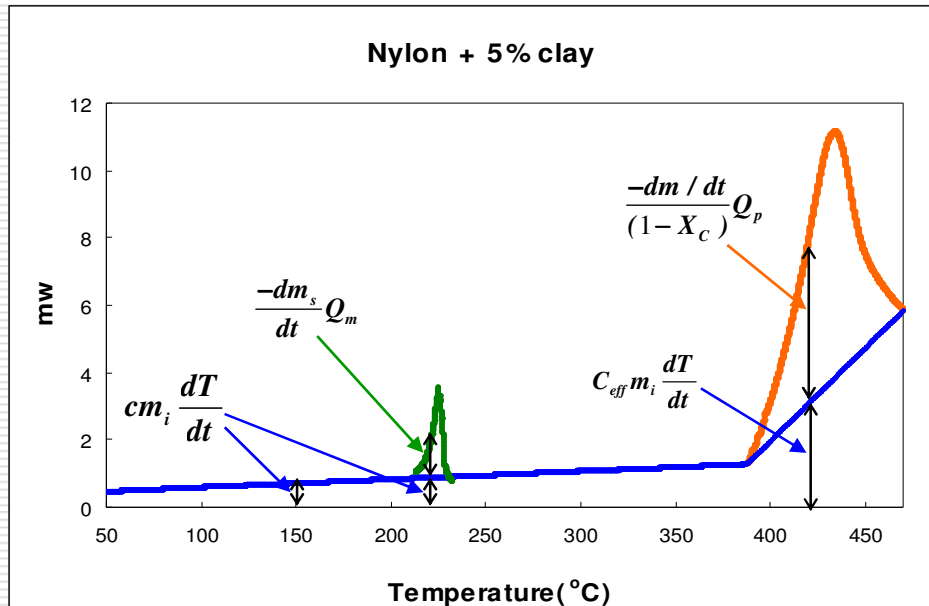


Figure 7. Sample signal of Nylon+5% clay

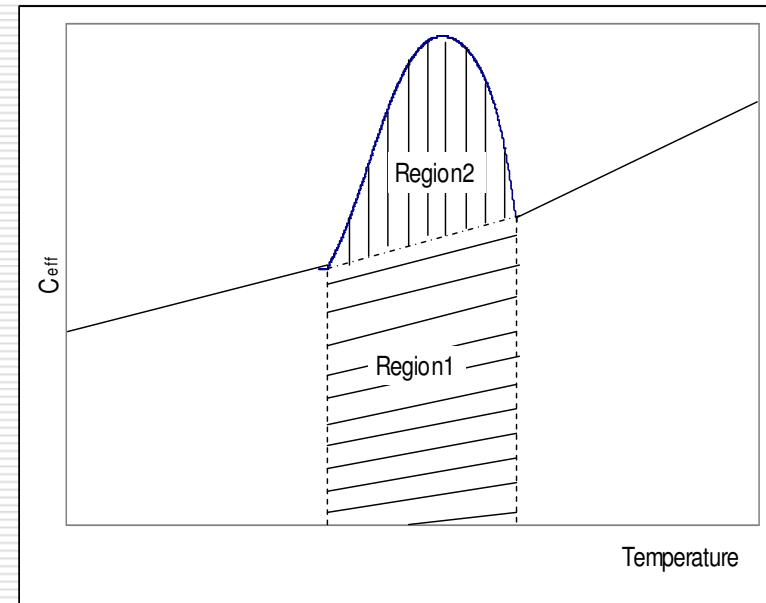


Figure 8. The effective  $c_p$

$$c_{eff} = \frac{\dot{Q}}{m_i \beta}$$

$$= \frac{1}{m_i} \int_{m_i}^{m_f} \frac{(-dm)}{(1-X_c)} Q_p + \int c dT$$

$$= Q_p + \int c dT$$

## Results of DSC analysis-2

	Values measured		Values selected in modeling	
	Nylon	Nylon +5 % Clay	Nylon	Nylon +5 % Clay
Heat of Melting, kJ/g	32, 35	35, 73	35	73
Heat of Decomposition, kJ/g active	388, 549	522, 557, 618, 671	550	670
Specific Heat of Solid, J/g-K 50 – 220 °C	1.6 – 2.5	1.5 – 2.5	$1.12 + 0.0075(T-T_{\infty})$	$1.21 + 0.0073(T-T_{\infty})$
Specific Heat of Melt, J/g-K 220 – 400 °C (decomposition 400 – 450 °C)	2.5 - 4	2.5 - 4	$-82 + 0.22(T-T_{\infty})$	$-79 + 0.21(T-T_{\infty})$

# Theory of the modeling

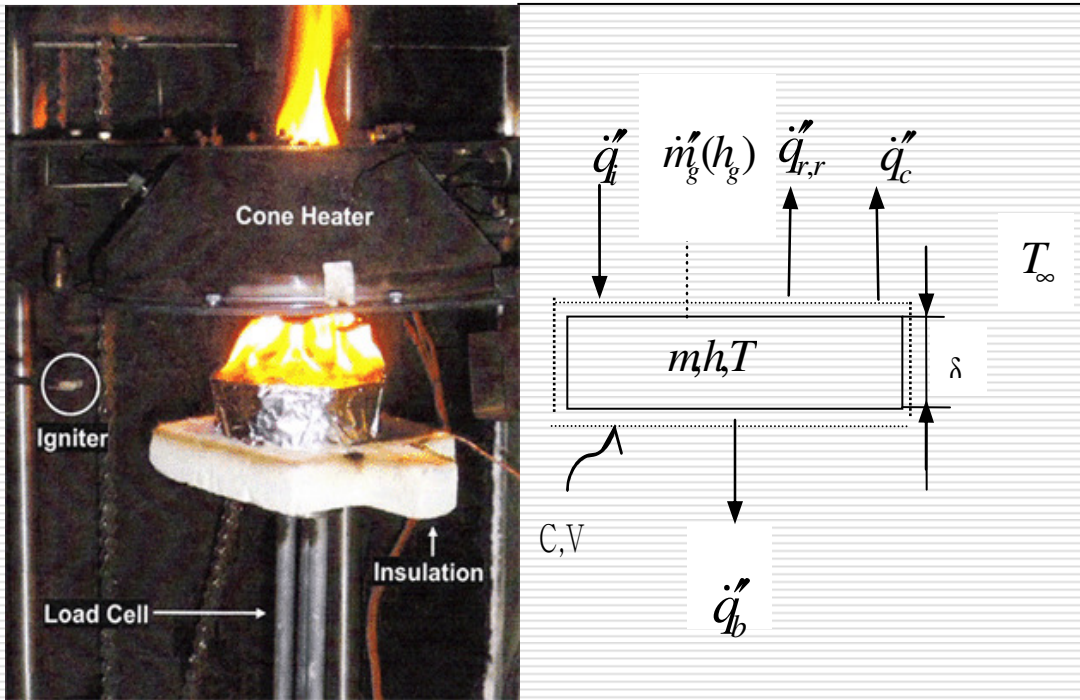
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- With kinetic and thermodynamic properties from TGA/DSC, the burning rate of thin polymers under radiant heat can be formulated.

The model results will be compared with the data from Cone Calorimeter experiments carried out by Xiu Liu

- The transient exposure and response of the thin material is divided into 4 phases
    - ✓ Pre-heating to melt
    - ✓ Melting phase
    - ✓ Decomposing to ignition
    - ✓ Flaming phase
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# Formulation of the model-1



- $\delta$  : Thickness of a material
- $\dot{q}''_i$  : Incident heat flux from the cone heater
- $\dot{q}''_f$  : Flame heat flux after flaming
- $\dot{q}''_c$  : Convective heating flux when no flame
- $\dot{q}''_{r,r}$  : Re-radiative heat flux to surroundings  $T_\infty$
- $\dot{q}''_b$  : Conductive heating flux to the insulator on the bottom

Cone calorimeter assembly & heating of material in C.V

✓ The general equation is

$$\rho c_p \delta \frac{dT}{dt} = \dot{q}'' + Q_m \frac{\rho \delta}{\Delta t_m} + Q_p \frac{d\rho}{dt} \delta$$

# Formulation of the Model-2

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□ The model is formulated from the conservation laws

■ Energy, mass, species(kinetics) conservation

1. Pre-heating

$$\rho c_p \delta \frac{dT}{dt} = \alpha \dot{q}_i'' - \epsilon \sigma (T^4 - T_\infty^4) - h_c (T - T_\infty) - \sqrt{\frac{\pi k' \rho' c_p'}{4t}} (T - T_\infty)$$

2. Melting :  $T_m$  is constant

$$\rho c_p \delta \frac{dT}{dt} = \alpha \dot{q}_i'' - \epsilon \sigma (T^4 - T_\infty^4) - h_c (T - T_\infty) - \sqrt{\frac{\pi k' \rho' c_p'}{4t}} - Q_m \frac{d\rho}{dt} \delta$$

3. Decomposing

✓ Energy conservation

$$\rho c_p \delta \frac{dT}{dt} = \alpha \dot{q}_i'' - \epsilon \sigma (T^4 - T_\infty^4) - h_c (T - T_\infty) - \sqrt{\frac{\pi k' \rho' c_p'}{4t}} (T - T_\infty) + Q_p \frac{d\rho}{dt} \delta$$

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# Formulation of the Model-3

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- ✓ Kinetics of decomposition

$$\frac{d\rho}{dt} = -\rho_a a_p \exp(-E_a/R \cdot T)$$

- ✓ Mass conservation

$$\frac{d\rho}{dt} = (1 - X_c) \frac{d\rho_a}{dt}$$

## 4. Flaming burning

- ✓ Energy conservation

$$\rho c_p \delta \frac{dT}{dt} = \alpha \dot{q}_i'' + \dot{q}_f'' - \varepsilon \sigma (T^4 - T_\infty^4) - \sqrt{\frac{\pi k' \rho' c'_p}{4t}} (T - T_\infty) + Q_p \frac{d\rho}{dt} \delta$$

- ✓ Decomposition Kinetics
- ✓ Mass conservation

❖ These equations were solved by Mathematica.

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# Modeling: ignition and burning

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- Flash-point using the criteria, 13 kW/m<sup>2</sup>  
 $\dot{m}_g'' = 0.46 \text{ g/m}^2\text{s}$ , at  $T_{flash}$
- Fire-point using the criteria, 50 kW/m<sup>2</sup>  
 $\dot{m}_g'' = 1.79 \text{ g/m}^2\text{s}$ , at  $T_{fire}$
- Flame heat fluxes coming from Cone Calorimeter data

	Nylon	Nylon+5%clay
1.6mm	20 kW/m <sup>2</sup>	20kW/m <sup>2</sup>
3.2mm	30 kW/m <sup>2</sup>	18kW/m <sup>2</sup>

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# Heating Rates

- The heating rates employed by TGA were 1, 2, 5, 10°C/min whereas the heating rates in the Cone Calorimeter experiments are relatively high. It is relevant to real fire

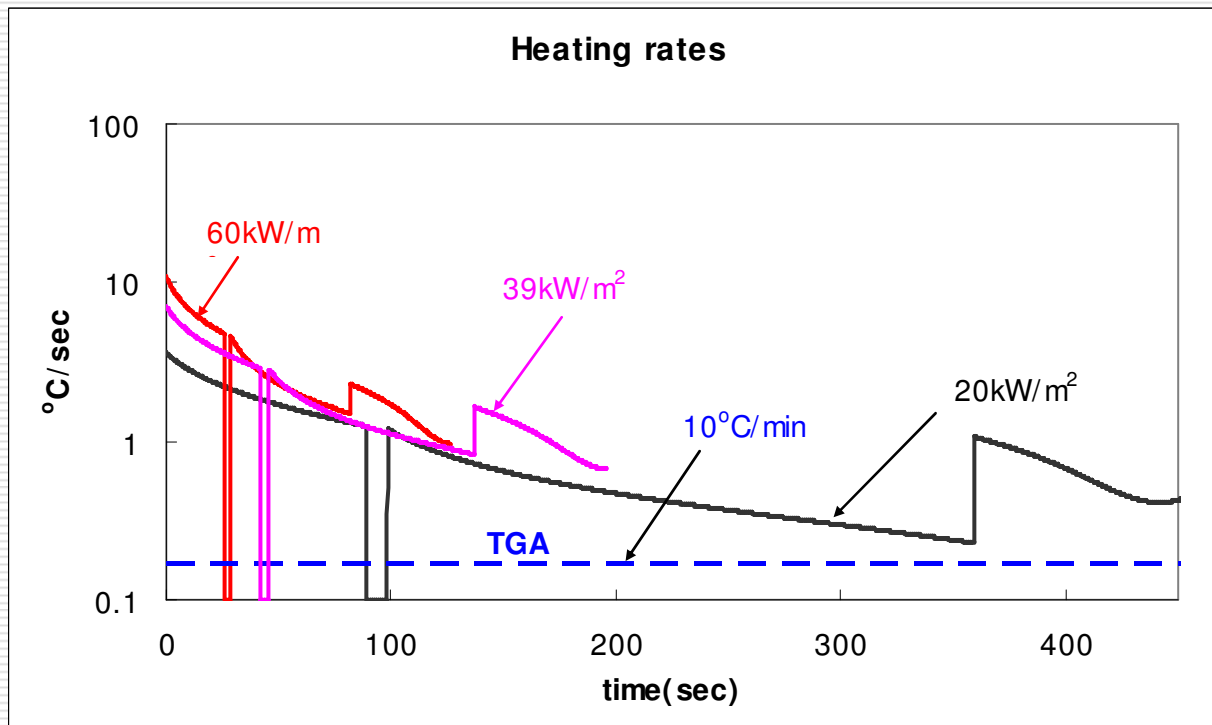


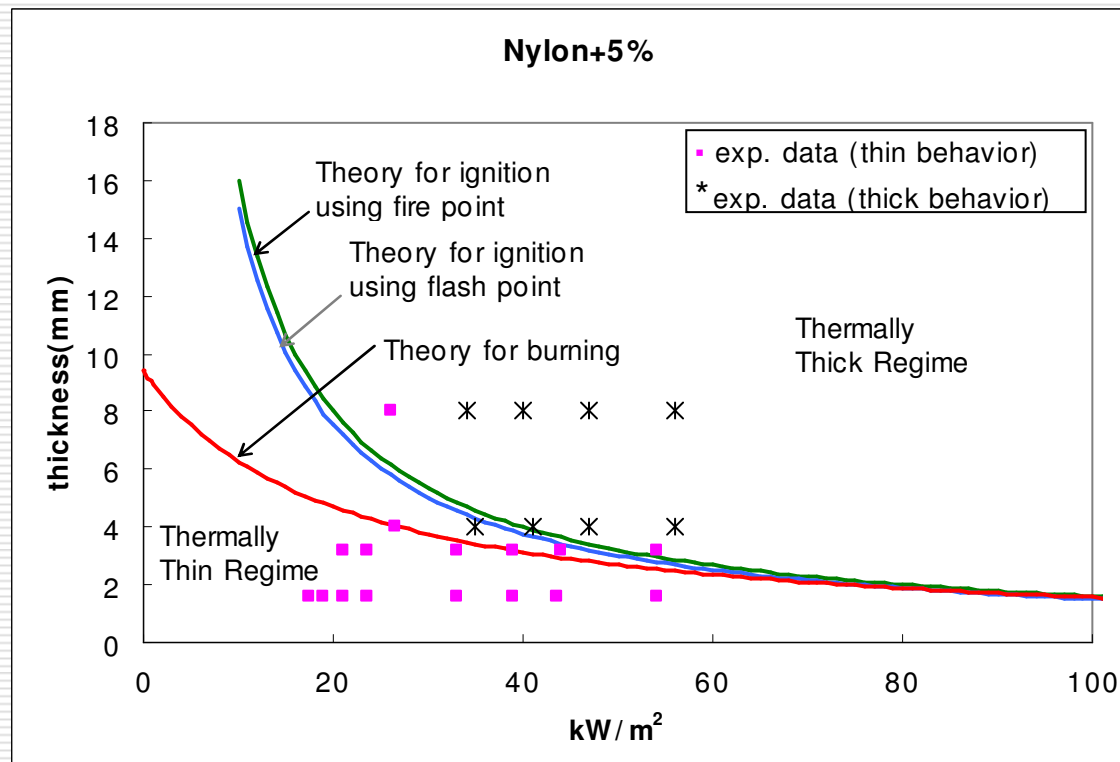
Figure 9. The heating rates in the TGA, and Cone Calorimeter

# The criteria of thermally thin

□ What is the criteria of thermally thin burning?

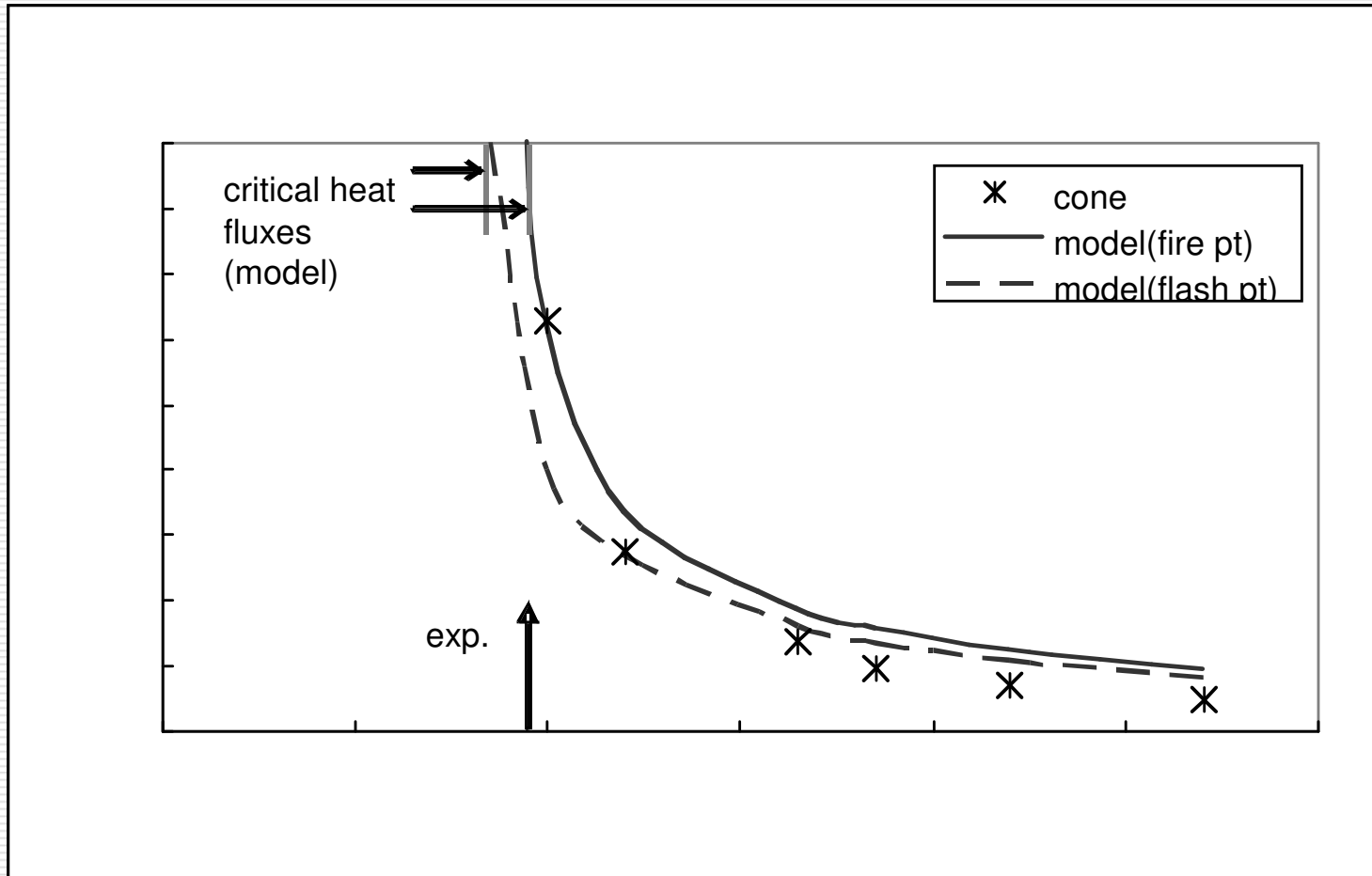
✓ A criteria for thermally thin ignition :  $l_{thin} = 2 \frac{k(T_{ig} - T_o)}{\dot{q}_i''}$

✓ A criteria for thermally thin Burning :  $\delta_s = \frac{2k(T_p - T_\infty)}{\dot{q}_{net}''}$



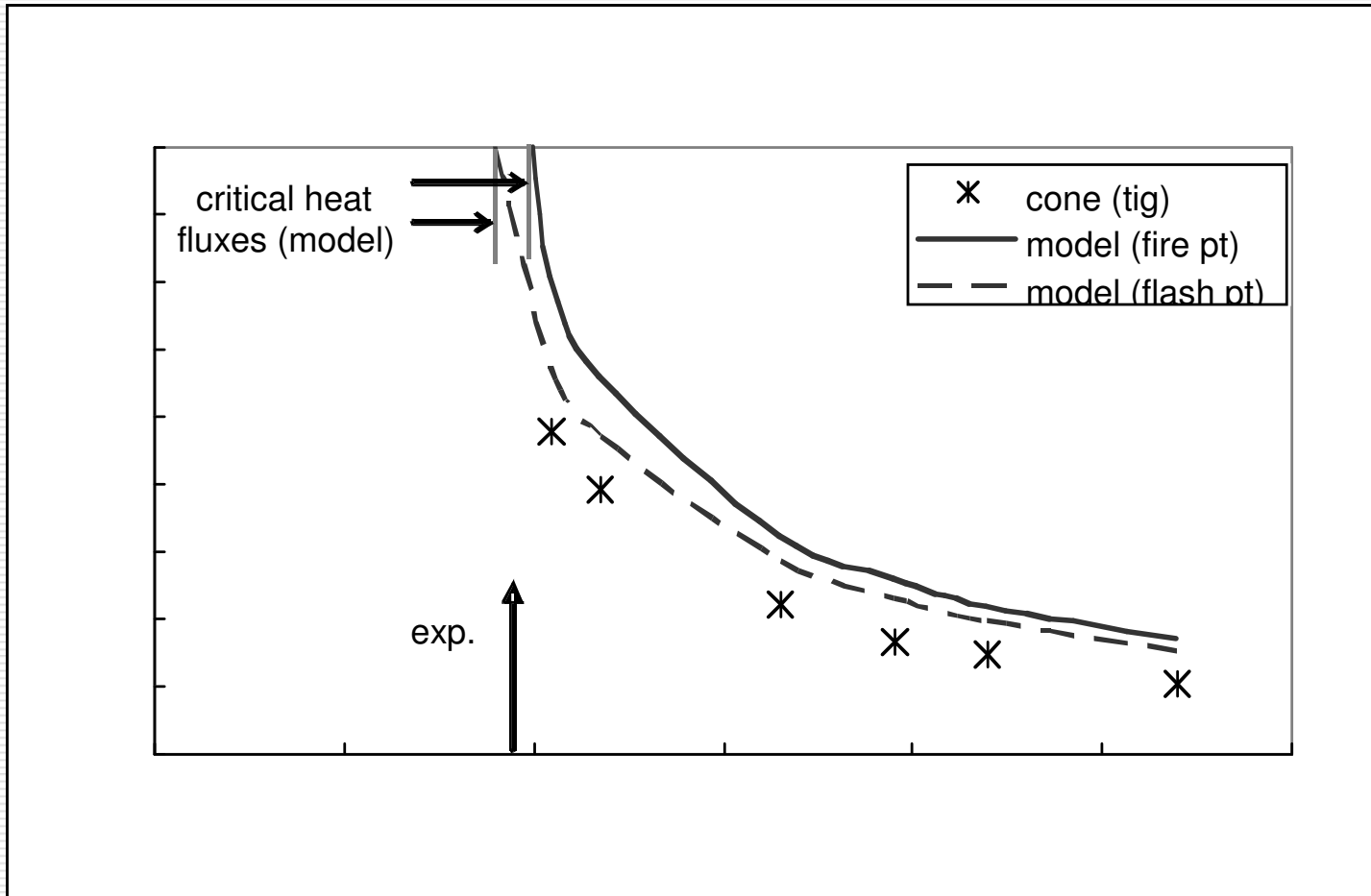
# Prediction of Ignition

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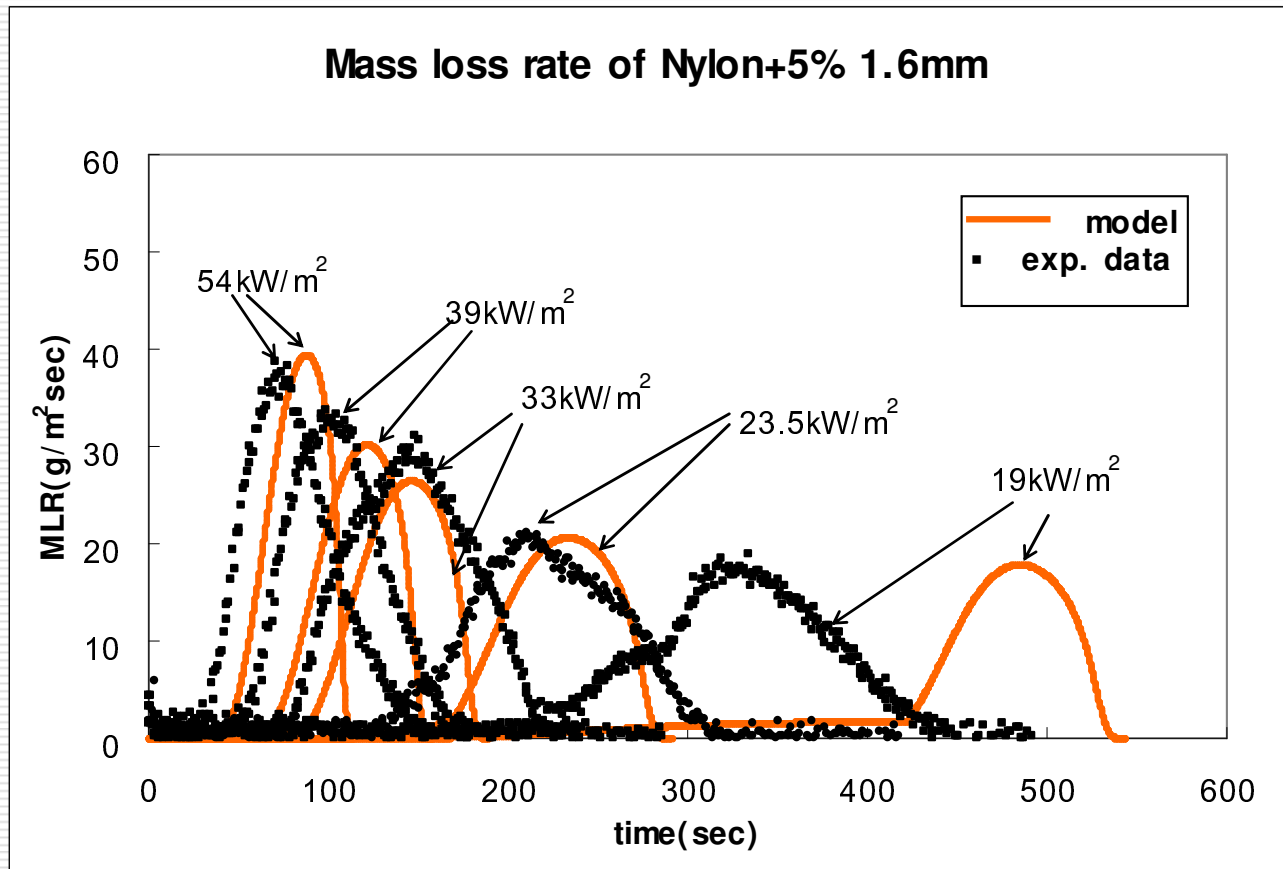
# Ignition-2

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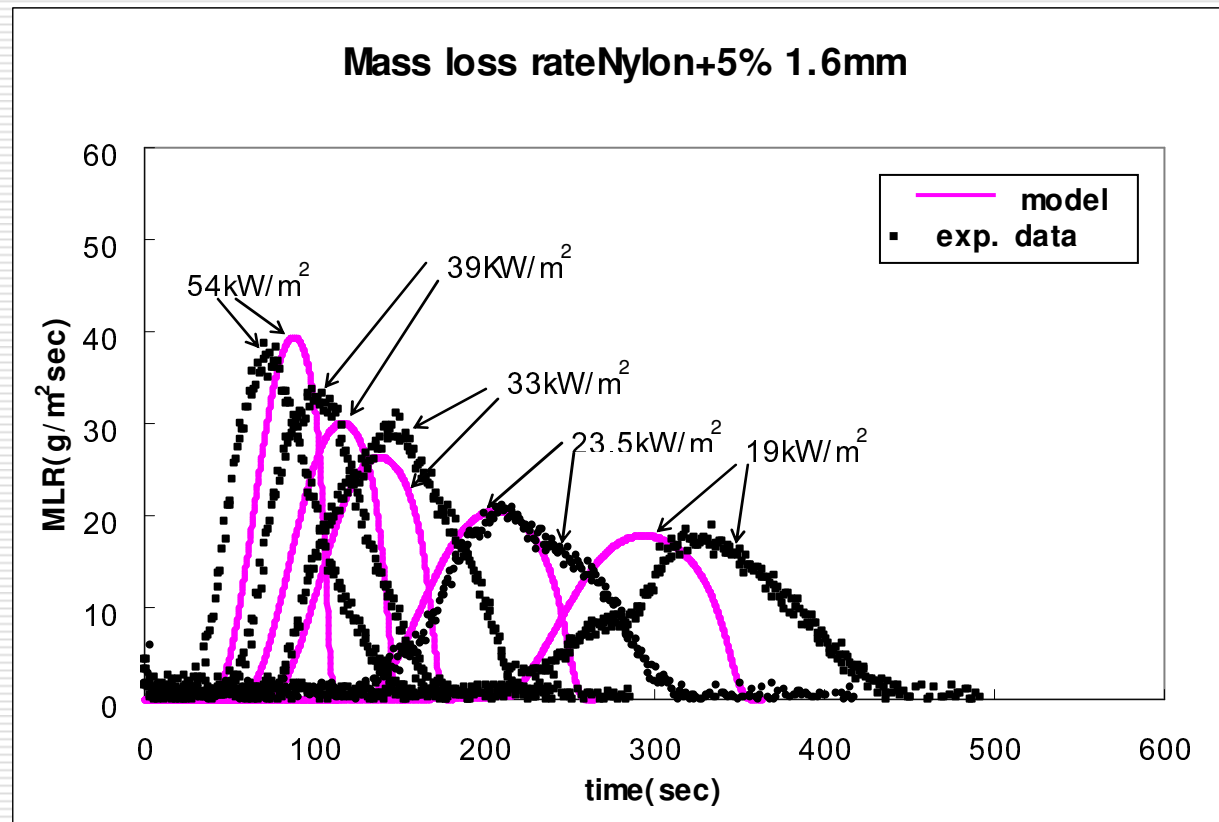
# Comparing the model to the cone calorimeter data

Flaming initiated at the fire point



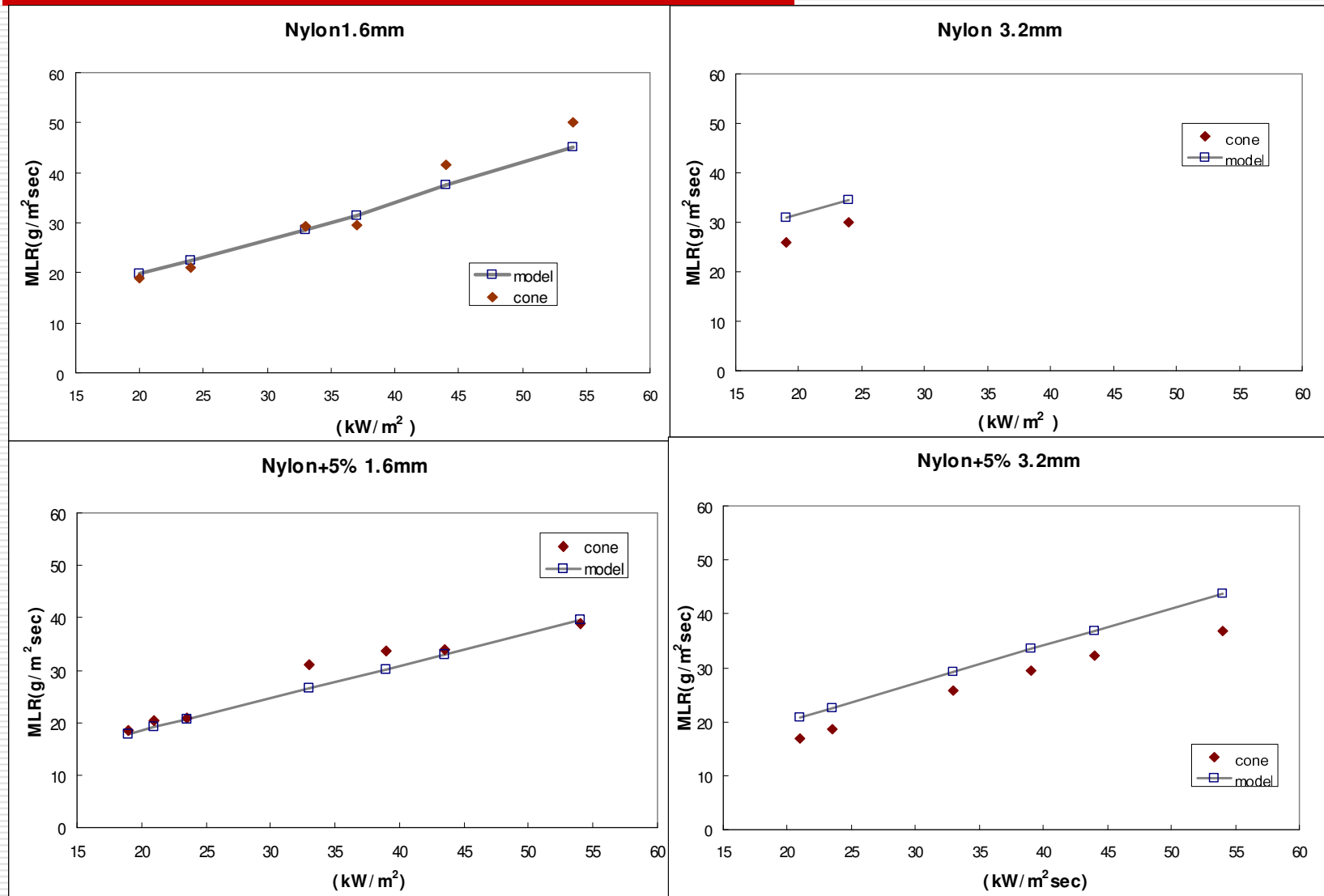
# Comparing the model to the cone calorimeter data

Flaming initiated at the flash point





# Modeling Result: Peak Average Burning Rate



## *T<sub>flash</sub> & T<sub>fire</sub>*

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- The flash point and fire point calculated by the model are found to be nearly constant over the heat flux range: 19 kW/m<sup>2</sup> to 54 kW/m<sup>2</sup>.

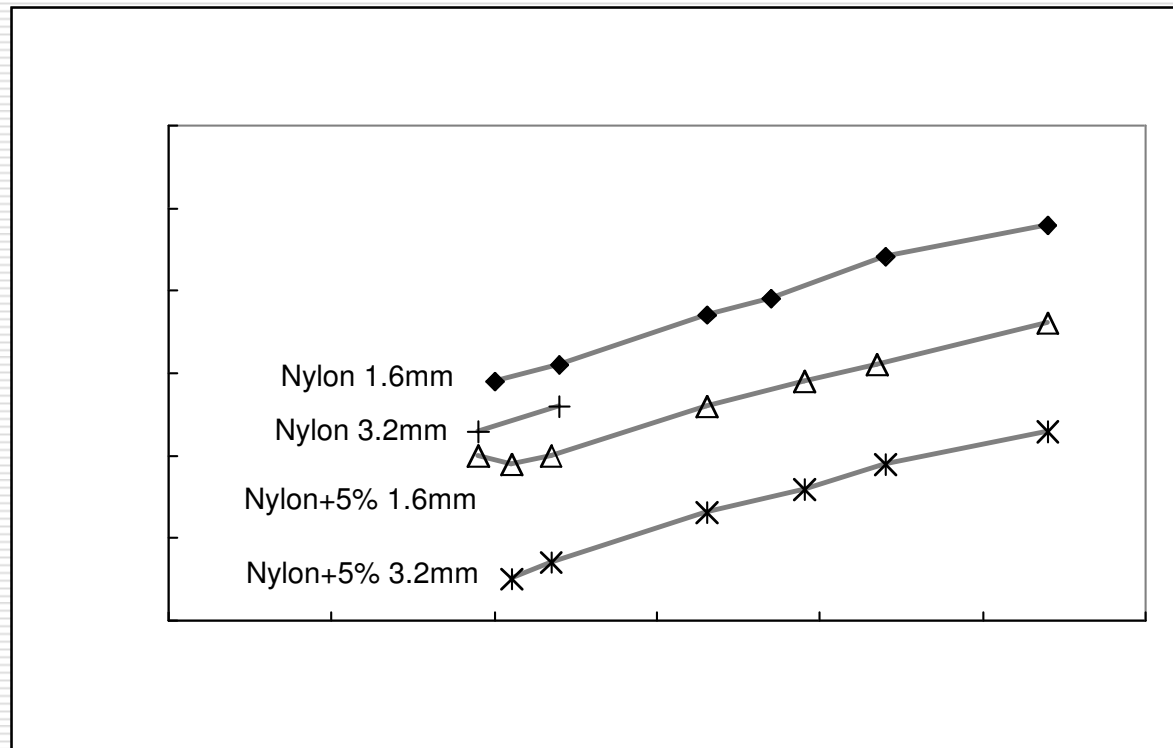
	Nylon 1.6 mm	Nylon 3.2 mm	Nylon+5% clay 1.6 mm	Nylon+5% clay 3.2 mm
Flash-point	383 °C	372 °C	378 °C	367 °C
Fire-point	406 °C	394 °C	403 °C	388 °C

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# Decomposition temperature

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- In contrast, the temperature ( $T_p$ ) on the peak burning rate increases with the radiation heat flux.



## Conclusions

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- ✓ The theoretical results for thermally thin ignition and burning yield good agreement with data for 1.6 mm samples of Nylon and Nylon with 5 % nano-clay.
  - ✓ TGA and DSC data provide a good basis for the theory, but reveal no distinct differences between the pure Nylon and the nano-clay Nylon within the accuracy of the data.
  - ✓ Hence, the inhibiting nature of the nano-clay appears to be solely that of the insulating char layer that is more significant for thick samples.
  - ✓ The Nylon sample is thermally thin up to about 3.2 mm.
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# END

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